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GHGT-12

Accelerated MEA degradation study in hybrid CO₂ capture systems

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Abstract

CO₂ capture systems are typically divided into pre- post- and oxyfuel- combustion systems. However, the interest on hybrid systems, which integrate elements of more than one of the above systems, is attracting major attention in recent times due to the potential higher energy efficiency. In this work, degradation studies have been conducted to identify operational issues related to amines degradation. Oxidative MEA degradation in presence of flue gas resembling oxygen enriched combustion has been investigated. MEA loss was 27% when flue gas with 15% CO₂ was used at 70°C, while only 20% loss was found in the presence of 50% CO₂, indicating that hybrid CO₂ capture systems may be used to decrease amine degradation of traditional post-combustion technologies. N-(2-hydroxyethyl)piperazin-3-one, N-(2-hydroxyethyl)-2-(2-hydroxyethylamino) acetamide, 2-oxadolidone, N-(2-hydroxyethyl)imidazole and N-N'-bis(2-hydroxyethyl)oxamine have been identified as MEA degradation products.

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Keywords: CCS, CO₂ capture, amine degradation, hybrid systems.

1. Introduction

Post-combustion capture using chemical absorption by aqueous amine-solutions is the most mature and industrially developed CO₂ capture technology.

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The amine-based chemical absorption process has been used in CO₂ and H₂S removal from gas-treating plants for decades [1]. Monoethanolamine (MEA) is considered as a benchmark solvent, as it is widely used due to its high cyclic capacity, significant absorption-stripping kinetic rates at low CO₂ concentration and high water solubility [1]. However, the high energy penalty related to amines regeneration and solvent degradation represent key issues hindering a large deployment of this technology. Moreover, the operating costs related to amine degradation have been estimated to be around 10% of the total CO₂ capture cost [2].

Degradation studies have been conducted to identify potential environmental and operational issues related to amine degradation compounds [1,3]. The authors have recently conducted a review of amine degradation processes [4]. Two main types of amine degradation have been identified: 1) thermal degradation and, 2) oxidative degradation in which O₂ participates [4, 5]. Oxidative degradation occurs in the presence of O₂, which will react with MEA to produce ammonia and other products more corrosive than the starting amine. Dissolved oxygen that does not react in the absorber will react in the cross exchanger or the stripper, where the temperature is 100-120°C [5]. This type of degradation has become a key issue in chemical absorption process for the CO₂ separation from the flue gas in fossil fuels power plants, where the O₂ concentration varies typically between 3-5%. Oxidative degradation can be decoupled from thermal degradation by operating at 40-70°C [6,7]. Oxidative degradation is a very slow process, where a typical test lasts for about 4 weeks [8], so that semi-batch experiments have been used to simulate the conditions of oxidative degradation in the absorber, where flue gas containing excess oxygen from combustion continuously contacts the charged amine [3]. Liquid Chromatography combined with Mass Spectrometry (LC-MS) is typically used to quantify amine concentration remained in the solution [8] and can also be used to quantify degradation products with molecular weight higher than 50 a.m.u. For compounds with lower than 50 a.m.u., GC-MS is used [9].

Recently, hybrid systems that link different elements among the main CO₂ capture systems have been proposed. It has been suggested that these systems such as post-combustion capture with oxygen enriched combustion, may be cheaper and more energy efficient than traditional CO₂ capture systems [10]. Therefore, this work focus on the investigation of oxidative MEA degradation in presence of flue gas with higher CO₂ concentration than traditional air-fired boilers, resulting from oxygen enriched combustion [11].

2. Method

The degradation studies were carried out for 30 days at 70°C, 1bara, using synthetic flue gases with 15 or 50 vol.% CO₂ and 3 or 6vol.% O₂, balanced with N₂. The oxidative degradation set-up consisted of a 500 mL 3-neck stirred flask, where the 5M MEA solutions were exposed to the specific gases above-mentioned and stirred at 900 rpm.

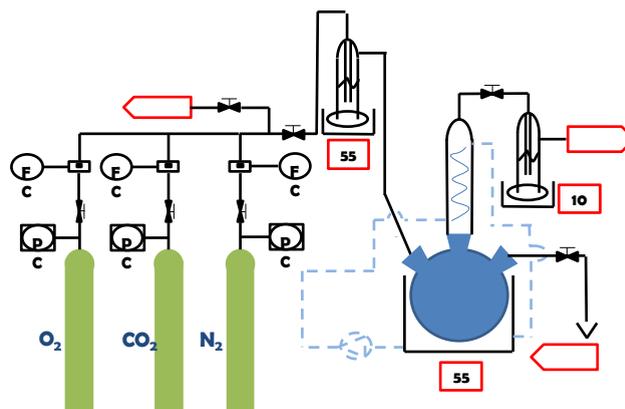


Figure 1 MEA degradation apparatus.

The gases leaving the gas cylinders (1L/min) were saturated with water before being introduced into the 3-neck stirred flask. The experiment was carried out in a fume cupboard. 5-ml samples were withdrawn every 3 days using a glass syringe to be analyzed.

The measurements of the MEA concentration change and the identification of the degradation products were carried out using a Liquid Chromatograph (LC). A LC-MS/MS equipment 6460 Triple Quadrupole MS coupled with 1290 Infinity LC Chromatography and Infinity auto sampler 1200 series G4226A from Agilent Technologies was used. The molecules were ionized by an electrospray ionization source (ESI). The column used was an Ascentis Express RP-Amide HPLC Column with dimensions: 15 cm x 4.6 mm; 2.7 microns; CAT#53931-U, using 25 mM formic acid in water as eluent (0.6 mL/min). 25 mM acid formic in water was required as eluent.

Calibration curves were obtained using standard solutions containing 10, 15, 20, 25, 30, 35, 40, 45, 50 ppm MEA with internal standard solution of 20 and 40 ppm MEA. LC samples were prepared diluting 100 μ l in 10 ml for two times and the injection volume was 10 μ l.

3. Results

3.1. Amine degradation

The degradation studies show that the O₂ partial pressure affects significantly the amine degradation. Intermediate solution concentrations, as that used in this work (5M), exhibit the effects of both kinetics and O₂ mass transfer control on MEA degradation rate [12]. To eliminate any mass transfer resistance, the solutions were vigorously stirred at 900rpm during the laboratory experiments. Temperature was set at higher temperature compared to that found in absorption columns typically employed for these applications [13-15]. The temperature increase from the typical 50°C was used to speed up the degradation process and reduce the experimental time up to 30 days. Figure 1 shows the MEA degradation over 30 days. In presence of high CO₂ concentration (50vol.%), the solubility and diffusion coefficient of O₂ decrease, and consequently, the amine degradation rates decrease as well, as previously suggested [16]. MEA losses were 27% and 17% in presence of 15% and 50% CO₂ in 3%-O₂ concentrated flue gas, respectively. The degradation increased by 7% and 23%, when the O₂ content was 6% instead of 3%. The presence of higher O₂ concentration in the flue gas strengthened kinetic and O₂ diffusion into the solution, limiting the benefits that the presence of higher CO₂ concentration in the flue gas produced on oxidative degradation process.

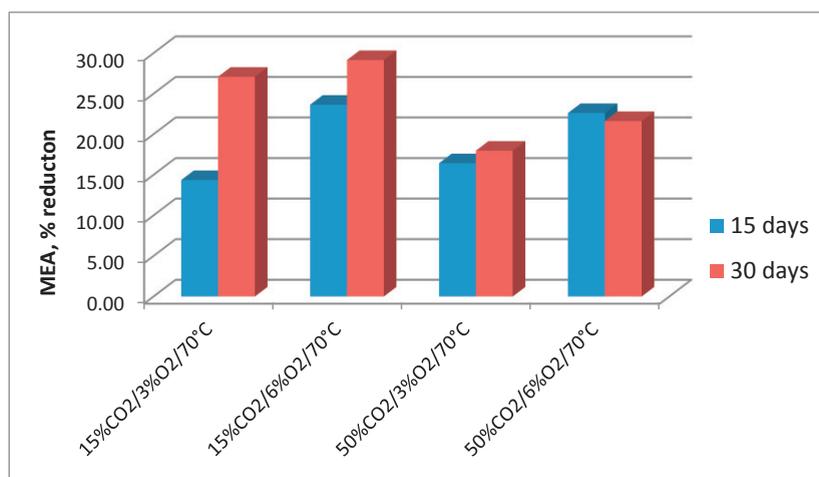


Figure 2 MEA degradation over 30 days.

Although it seems that higher CO₂ concentration in the flue gas avoids partially oxidative degradation, it should be noticed that more than 90% of the total degraded amine was achieved in presence of 50% CO₂ after 15 days, whereas experiments in presence of 15% CO₂ required more time to achieve same level of degradation.

3.2. Degradation products

The method used was not able to identify low molecular weight MEA degradation products such as ammonia, formic acid, acetic acid. However, some high molecular weight compounds were identified. The main degradation products identified by LC-MS were HEPO (N-(2-hydroxyethyl)piperazin-3-one) and HEHEAA (N-(2-hydroxyethyl)-2-(2-hydroxyethylamino) acetamide). The HEHEAA signal intensity increase from day 3 to day 18, and then it decreases indicating its conversion in HEPO [17,18]. This phenomena agrees with the mechanisms proposed by Supap and Arduengo that indicates HEPO formation by dehydration of HEHEAA [16,17]. Other compounds such as OZD (2-oxadolidone), HEI (N-(2-hydroxyethyl)imidazole) and BHEOX (N-N'-Bis(2-hydroxyethyl)oxamine) were also identified.

Table 1. Identified degradation products.

Main Degradation Product	Abbreviation	MW
2-oxazolidone	OZD	87
N-(2-hydroxyethyl)imidazole	HEI	112
N-(2-hydroxyethyl)piperazin-3-one	HEPO	144
N-(2-hydroxyethyl)-2-(2-hydroxyethylamino)acetamide	HEHEAA	162
N,N'-Bis (2-hydroxyethyl)oxamide	BHEOX	176

4. Conclusions

The degradation of MEA during CO₂ capture in hybrid post-combustion capture with oxygen enriched combustion has been studied. Presence of oxygen and temperatures over 50°C shortened the amine degradation experiments that typically require several weeks or the presence of degradation promoters to be studied. MEA loss was 27% when flue gas contained 15% CO₂. HEPO and HEHEAA, OZD, HEI and BEHOX were identified as MEA degradation products under the studied conditions. The degradation increased by a maximum of 23%, when the O₂ content was 6% instead of 3%. This work indicates that hybrid CO₂ capture systems may be used to decrease the amine degradation of traditional post-combustion technologies and related costs.

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References

- [1] Kohl AL, Nielsen RB, Gas purification, 5th edition, 1997, Gulf Publishing Company, Houston, USA.
- [2] Fredriksen SB, Jens KJ, Oxidative degradation of aqueous amine solutions of MEA, AMP, MDEA, Pz: A review, Energy Procedia 2013; 37: 1770-1777.
- [3] Voice AK, Cloosmann F, Rochelle GT, Oxidative Degradation of Amines With High-Temperature Cycling, Energy Procedia 2013; 37: 2118-2132.
- [4] Vega F, Sanna A, Cortés V, Navarrete B, Maroto-Valer MM, Degradation of amine-based solvents in CO₂ capture process by chemical absorption. Greenhouse Gases: Science and Technology 2014; DOI: 10.1002/ghg.1446.
- [5] Bedell SA, Oxidative degradation mechanisms for amines in flue gas capture, Energy Procedia 2009; 1:771-778.
- [6] Voice AK, Rochelle GT, Oxidation of amines at absorber conditions for CO₂ capture from flue gas, Energy Procedia 2011; 4:171-178.
- [7] Freeman SA, Davis J, Rochelle GT. Degradation of aqueous piperazine in carbon dioxide capture. International Journal of Greenhouse Gases Control 2010; 4:756-761.
- [8] Lawal O, Bello A, Idem R. The Role of Methyl Diethanolamine (MDEA) in Preventing the Oxidative Degradation of CO₂ Loaded and Concentrated Aqueous Monoethanolamine (MEA)-MDEA Blends during CO₂ Absorption from Flue Gases. Industrial and Engineering Chemistry Research 2005; 44:1874-1896.
- [9] Lepaumier H et al., Comparison of MEA degradation in pilot-scale with lab-scale experiments, Energy Procedia 2011;4:1652–1659.
- [10] Favre E, Bounaceur R, Roizard D, A hybrid process combining oxygen enriched air combustion and membrane separation for post-combustion carbon dioxide capture, Separation and Purification Technology 2009;68:30–36.
- [11] Huang Y, Wang M, Stephenson P, Rezvani S, McIlveen-Wright D, Minchener A, Hewitt N, Dave A, Fleche A. Hybrid coal-fired power plants with CO₂ capture: A technical and economic evaluation based on computational simulations. Fuel 2012;101:244–253
- [12] Goff GS, Oxidative Degradation of Aqueous MEA in CO₂ Capture Processes: Iron and Copper Catalysis, Inhibition and O₂ Mass Transfer, Ph.D. Dissertation, The University of Texas at Austin, May 2005.
- [13] Kvamsdal HM and Rochelle GT. Effects of the temperature bulge in CO₂ absorption from flue gas by aqueous Monoethanolamine. Ind. Eng. Chem. Res. 2008; 47: 867 – 875
- [14] Mangalapally HP and Hasse H. Pilot plant study of two new solvents for post combustion carbon dioxide capture by reactive absorption and comparison to monoethanolamine. Chemical Engineering Science. 2011; 66: 5512–5522
- [15] Mangalapally HP, Notz R, Asprion N, Sieder G, Garcia H, Hasse H. Pilot plant study of four new solvents for post combustion carbon dioxide capture by reactive absorption and comparison to MEA. International Journal of Greenhouse Gas Control. 2012; 8: 20512;
- [16] Goff GS, Rochelle GT, Monoethanolamine Degradation: O₂ Mass Transfer Effects under CO₂ Capture Conditions, Ind. Eng. Chem. Res. 2004;43:6400-6408.
- [17] Supap T, Idem R, Tontiwachwuthikul P and Saiwan C. Kinetics of sulfur dioxide- and oxygen-induced degradation of aqueous monoethanolamine solution during CO₂ absorption from power plant flue gas streams. Int. J. Greenh. Gas. Con. 2009;3:133-142.
- [18] Arduengo AJ, Gentry FP, Taverkere PK and Simmons H, Process for manufacture of imidazoles. US Patent No. 6177575 B1 (2001).