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## Monitoring the electrical properties of metal ore mine tailings during sedimentation

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1 **Monitoring the electrical properties of metal ore mine tailings during**  
2 **sedimentation**

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23

24 ABSTRACT

25 Material characterisation and process monitoring in particulate media can be enhanced by measuring  
26 electric properties. In this study, the temporal changes in electrical resistivity were recorded during  
27 the sedimentation of gold and copper mine tailings (i.e. crushed rock particles deposited as a slurry).  
28 A small sedimentation column, fitted with four sets of electrodes, was used to perform undrained  
29 settling tests on slurries with solids contents over the range 50%-65%. It was observed that during  
30 sedimentation, the electrical resistivity increased to a constant steady-state value as the porosity of the  
31 slurry decreased. The data was modelled using Archie's law to highlight the effect of pore-fluid  
32 resistivity, porosity and tortuosity on the bulk resistivity of the tailings mass.

33

34 **KEYWORDS:** Contaminated material, fabric/structure of soils, strength and testing of materials.

35

## 36 **1 INTRODUCTION**

37 European Directive 2006/21/EC of the European Parliament and of the Council of 15 March 2006 on  
38 the management of waste from extractive industries EC (2006) requires the characterisation of the  
39 waste to be deposited in a storage facility in order to guarantee physical and chemical stability in the  
40 short and long term. Part of this characterisation process includes assessment of the geotechnical  
41 behaviour of the waste. For materials deposited as a slurry an important component of this assessment  
42 process consists of predicting the sedimentation and consolidation behaviour following deposition  
43 (Azam 2014a, 2014b).

44 During sedimentation, the waste solids will settle and leave a clear interface between the top of the  
45 settling mass and the supernatant fluid. This process is usually simulated in the laboratory by means  
46 of simple “jar settling tests”, normally conducted in hydrometer cylinders. Slurry is poured inside the  
47 cylinder and the position of the slurry-fluid interface monitored, in order to obtain an indication of  
48 settlement rate and a minimum settle density. The tests can be carried out with underdrainage to  
49 simulate the presence of a high-permeability drainage layer below the waste. In this case the test is  
50 referred as “drained settling test”. Otherwise, the test is known as an “undrained settling test”.

51 The measurement of the electrical properties of particulate media offers an elegant and simple way to  
52 characterise materials and monitoring physio-chemical processes (Wagner and Scheuermann 2017).

53 The subject has been explored in detail by Santamarina et al (2001), including the underlying  
54 principles and laboratory experimental techniques. In many instances, it is relatively simple to modify  
55 existing equipment to allow the electrical properties of geo-materials to be recorded whilst a test is  
56 conducted in the standard way.

57 This paper presents results from a laboratory-based study on the sedimentation of mine tailings (i.e.  
58 crushed rock particles deposited as a slurry) using a modified sedimentation column to perform  
59 undrained settling tests. Although results from electrical measurements recorded during sedimentation  
60 of soft sediments have been published (see, for example, Blewett et al 2001; Klein & Santamarina  
61 2005), the Authors are not aware of similar tests carried out on mine waste derived from the

62 extraction of mineral products. Given the considerable volume of mine tailings produced every year,  
63 the environmental issues associated with their handling and storage, and the requirement to properly  
64 characterise their geotechnical properties, it is difficult to deny the benefits of exploring simple  
65 measuring techniques to study settling processes that could be developed for use both in the  
66 laboratory and in the field.

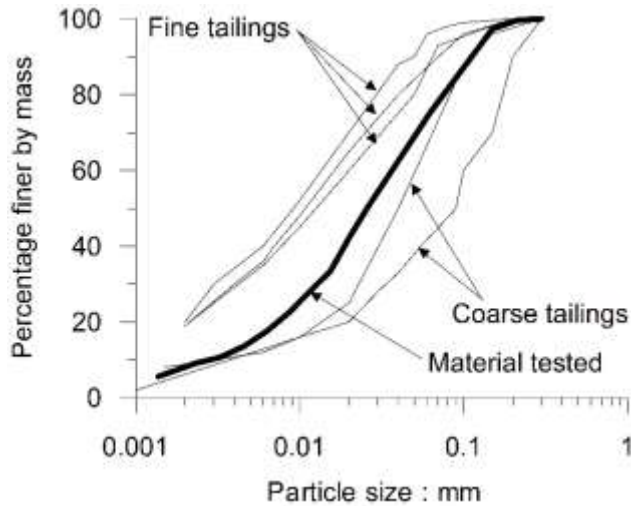
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## 68 **2 EXPERIMENTAL PROCEDURE**

### 69 **2.1 Material properties**

70 Gold and copper tailings were used in the current study. The Authors had access to a limited sample,  
71 which had previously been de-toxified for geotechnical laboratory work. The original material  
72 contained a mixture of coarse and fine particles and, as the original intention was to test the finer  
73 fraction (also known as ‘slimes’), material retained in the 0.3mm aperture sieve was discarded. The  
74 particle size distribution of the sample - obtained from a combination of wet sieving and  
75 sedimentation - is presented in Figure 1. The same figure also includes particle size distributions for  
76 fine and coarse gold and copper tailings taken from Blight (2010). It is evident that the particle size  
77 distribution of the selected material lies between the two sets of curves. Although not truly  
78 representative of fine tailings, it was decided to use this material in the study as further removal of  
79 coarser particles would have left too small a sample to perform the intended tests. The average specific  
80 gravity of the tailings, measured on a number of samples using a small pycnometer, was 2.88.

81



82

83 Figure 1. Particle size distribution of the tailings sample after removal of particles retained in the  
 84 0.3mm sieve. Also shown, curves for coarse and fine gold and copper tailings from Blight (2010).

85

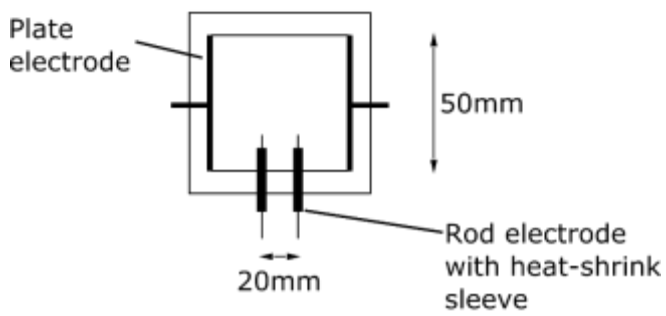
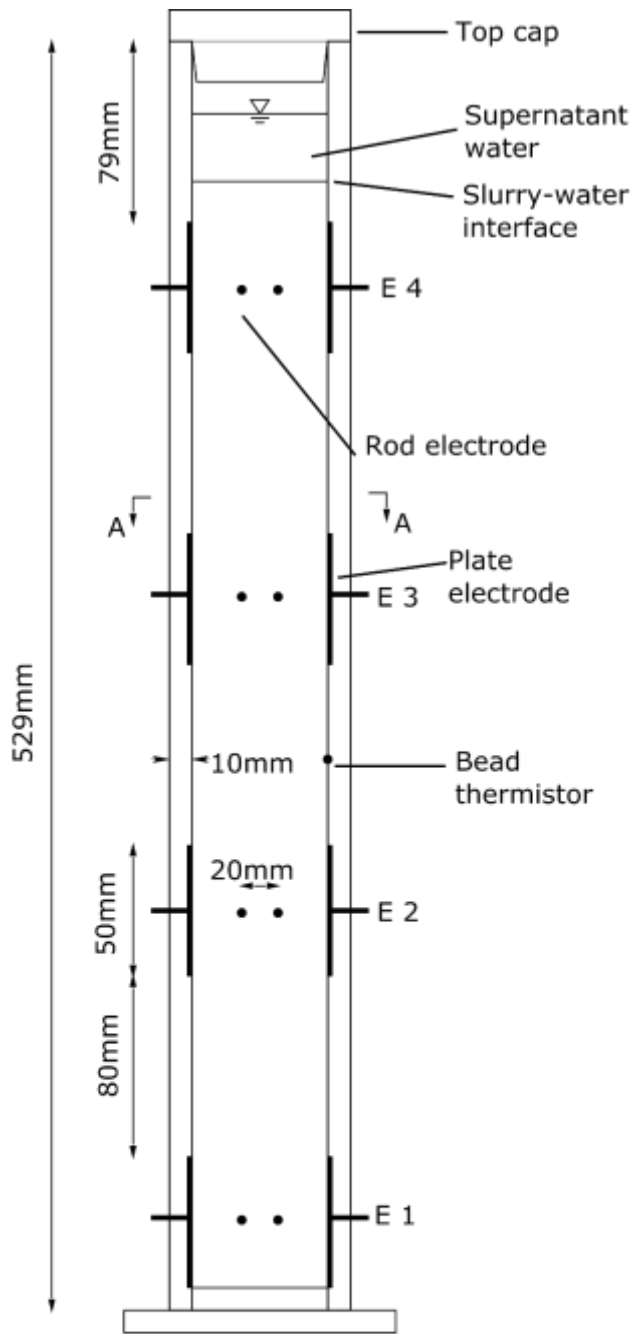
86 **2.2 Sedimentation column**

87 The sedimentation column used in the study was a modification of that used by Blewett et al (2001,  
 88 2003) to study the sedimentation of a kaolin slurry and monitor ionic migration through consolidated  
 89 kaolin. The acrylic column, shown in Figure 2, had internal dimensions of 50×50×519mm and  
 90 included four sets of electrodes, with the mid-height of each set located at 35mm, 165mm, 295mm  
 91 and 425mm above the base of the column. Each set of electrodes comprised a pair of 50×50mm  
 92 stainless steel (s/s) plates placed flush with the sides of the column, together with a pair of small  
 93 diameter (1.6mm) s/s rod electrodes. The rod electrodes were provided with heat-shrink sleeving to  
 94 expose a 6mm tip; the electrodes themselves were separated by a horizontal distance of 20mm and  
 95 protruded 12mm into the column.

96 The use of a four-terminal electrode arrangement, where the current electrodes (i.e. the s/s plates) and  
 97 potential electrodes (i.e the s/s rods) are separated, eliminates measurement errors due to electrode  
 98 polarization effects. As resistivity measurements are affected by temperature, a bead thermistor was  
 99 mounted in a side wall of the sedimentation column. This allowed continuous monitoring of the slurry  
 100 temperature, although tests were conducted in a temperature-controlled environment (20°C ± 2°C).

101 Electrical resistivity measurements were taken with an Agilent A4263B LCR meter set at a frequency  
102 of 1kHz with a signal amplitude of 100mV. Coaxial cables connected the measuring equipment to the  
103 electrodes; cable resistance was automatically nulled from the incoming data.

104



Section A-A

105

106 Figure 2. Sedimentation column showing location of electrodes (E1 to E4).



107

### 108 **2.3 Calibration of the sedimentation column**

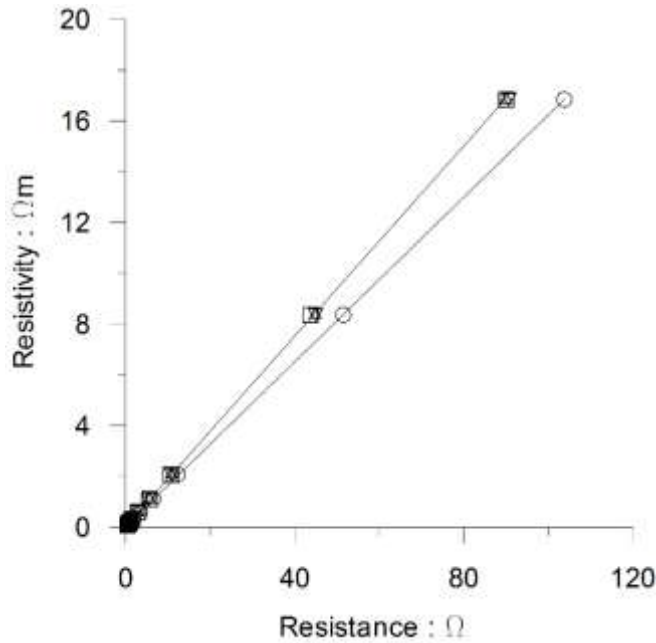
109 The bulk resistivity of a prismatic sample of slurry (denoted  $\rho_{mix}$ , in ohm-m) placed between a pair of  
110 electrodes (i.e. parallel electrical field lines) can be obtained from the expression

$$111 \quad \rho_{mix} = R \frac{A}{d} \quad (1)$$

112 where  $A$  is the electrode surface area ( $m^2$ ),  $d$  is the electrode separation (m) and  $R$  is the bulk  
113 resistance of the mixture (ohm). In a four-terminal electrode arrangement, such as that shown in  
114 Figure 2, the electrode separation  $d$  corresponds to the distance between rod electrodes, which can be  
115 measured. However, fringing effects will result in a non-parallel electrical field distribution between  
116 the plate electrodes and hence an enlargement of the area occupied by the electrical field. It is not  
117 possible to measure the value of  $A$  directly and it becomes necessary to obtain the geometrical  
118 constant  $A/d$  experimentally for each set of electrodes through calibration with a liquid of known  
119 resistivity. This was achieved by filling the sedimentation column with different molarities (hence  
120 resistivity) of salt (NaCl) solution and measuring the resistance at each electrode position.

121 A small cuboidal cell, capable of containing a sample of volumetric dimensions  $50 \times 50 \times 46$ mm and  
122 having an electrode arrangement similar to that used in the sedimentation column, was used to obtain  
123 the resistivity of NaCl solutions of different concentration, ranging from  $5 \times 10^{-3}$  to 2.0 mol/L (Note:  
124 this also covered the anticipated range of resistivity values for the tailings slurry). These values were  
125 then used to evaluate the geometrical constant  $A/d$  for each electrode set, which were: 0.1623m for  
126 position E1, 0.1898m for positions E2 and E3, and 0.1857m for position E4. The lower constant  
127 recorded at electrode position 1 (E1) results from the presence of the non-conductive boundary at the  
128 base of the column. Without fringing effects, the theoretical value of the geometrical constant for this  
129 electrode arrangement is 0.125m. The relationship between  $\rho$  and  $R$  obtained during the calibration  
130 process is presented in Figure 3.

131



132

133 Figure 3. Relationship between electrolyte resistivity  $\rho$  and resistance  $R$  recorded during calibration of  
 134 the sedimentation column and used to obtain the geometric constant  $A/d$  for each set of electrodes: E1  
 135 (○), E2 (□), E3 (Δ) and E4 (∇). Results for E2, E3 and E4 are virtually the same.

136

137 **2.4 Test procedure**

138 After initial sieving to remove material coarser than 0.3mm, the tailings were dried in an oven at  
 139 105°C and 2.3kg of dry material was mixed with sufficient deionised water to obtain a slurry with a  
 140 solids content,  $P$ , of 55%. The solids content, also known as pulp density or concentration, is given by  
 141 the mass of solids per kilogram of slurry. The mixture was placed inside a plastic container with an  
 142 airtight lid and left to hydrate for four days.

143 Following hydration, the slurry was first placed in a rotary mixer for 30 minutes and then poured  
 144 inside the sedimentation column. The 40mm gap left between the surface of the slurry and the top of  
 145 the column allowed an airtight cap to be placed, which ensured no loss of slurry during initial  
 146 agitation, as well as eliminating evaporative losses during the sedimentation stage. After vigorous  
 147 agitation of the column to ensure a homogeneous mix, it was placed on a laboratory bench and initial  
 148 readings of the height of the slurry, resistance at each electrode, and thermistor resistance taken.

149 Thereafter, values of the slurry-water interface height and electrode resistance were recorded;  
150 although no appreciable change in any of these quantities was observed after 4 to 5 hours, the test was  
151 conducted over a 24-hour period.

152 As only a limited mass of tailings was available for the study, following completion of the first test  
153 the material was dried at 105°C and reused in further tests. The same procedure was followed each  
154 time to monitor the sedimentation of slurries with solids contents of 50%, 52.5%, 55%, 57.5%, 60.5%  
155 and 65% (although tests were not performed in that order). Some of these solid contents are higher  
156 than values measured in the field, which range from 15% to 55% and are most commonly in the range  
157 of 40-55% (Vick 1990). However, it was noticed that when the solids content fell below 55% the  
158 slurry would settle below the third set of electrodes (E3 in Figure 2). Tests at higher solid contents  
159 allowed measurements to be recorded in three of the four electrode positions.

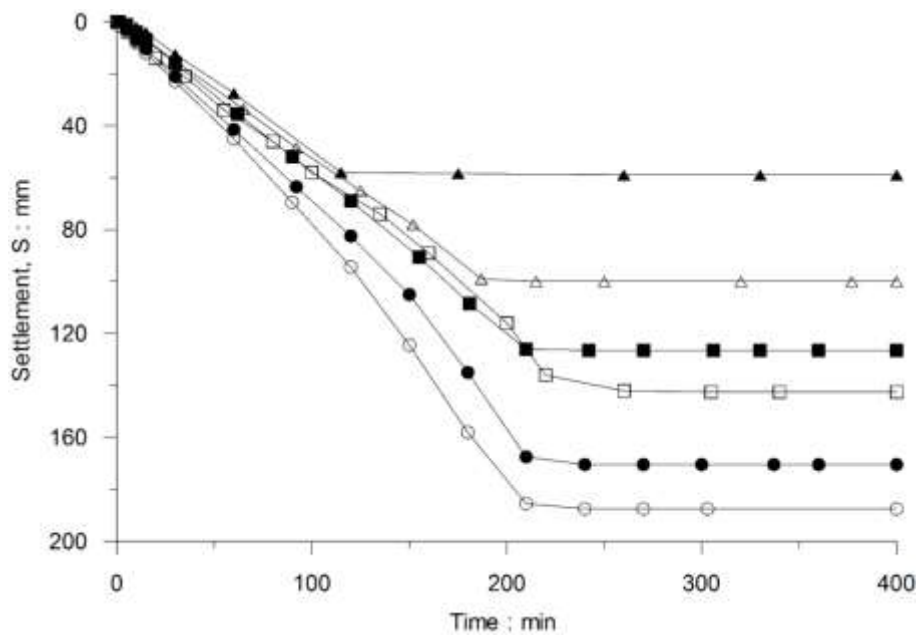
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## 161 **3 RESULTS**

### 162 **3.1 Sedimentation of slurry**

163 Shortly after the start of a test it was possible to identify an interface between the slurry and the  
164 supernatant liquid. The vertical movement of this interface is presented in Figure 4, where settlement  
165 corresponds to the vertical movement of the interface relative to the original height of slurry at the  
166 start of a test. In all cases, settlement occurred quickly and the slurry reached a stable condition after  
167 only a few hours as noted above. Although the curves plotted in Figure 4 have been terminated shortly  
168 after settlement ceased, measurements were continued for 24 hours, which showed no further  
169 movement beyond what is shown. Total settlements and true vertical strains as a function of solids  
170 content are presented in Figure 5. Initial and final average porosities of the tailings mass, together  
171 with changes in porosity during sedimentation, are shown in Figure 6.

172



173

174 Figure 4. Vertical settlement plotted against time for different solids contents: 50% (○), 52.5% (●),

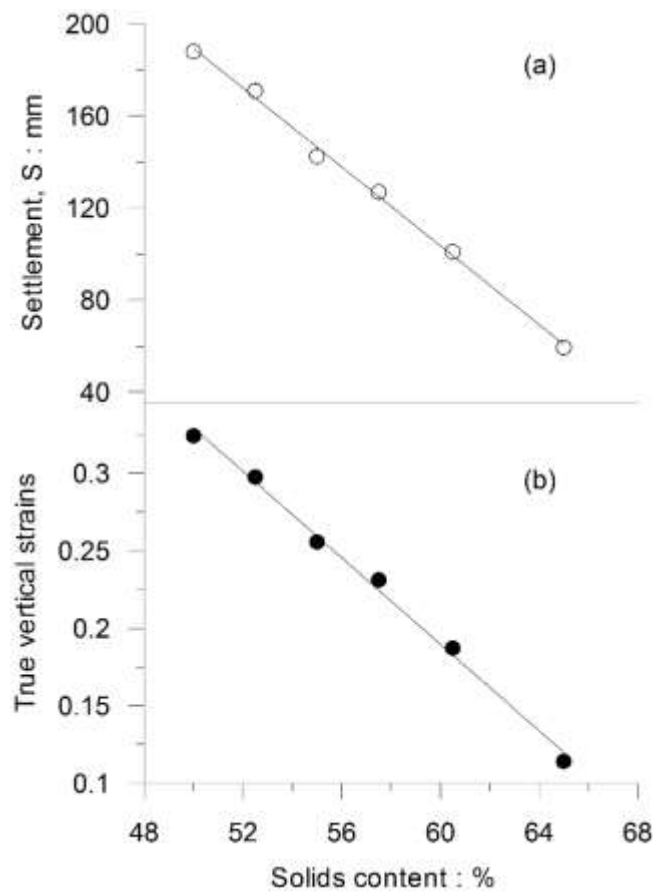
175 55% (□), 57.5% (■), 60.5% (Δ), and 65% (▲). Settlement refers to the vertical movement of the

176 slurry-water interface with respect to the original position of the slurry surface at the start of a test.

177

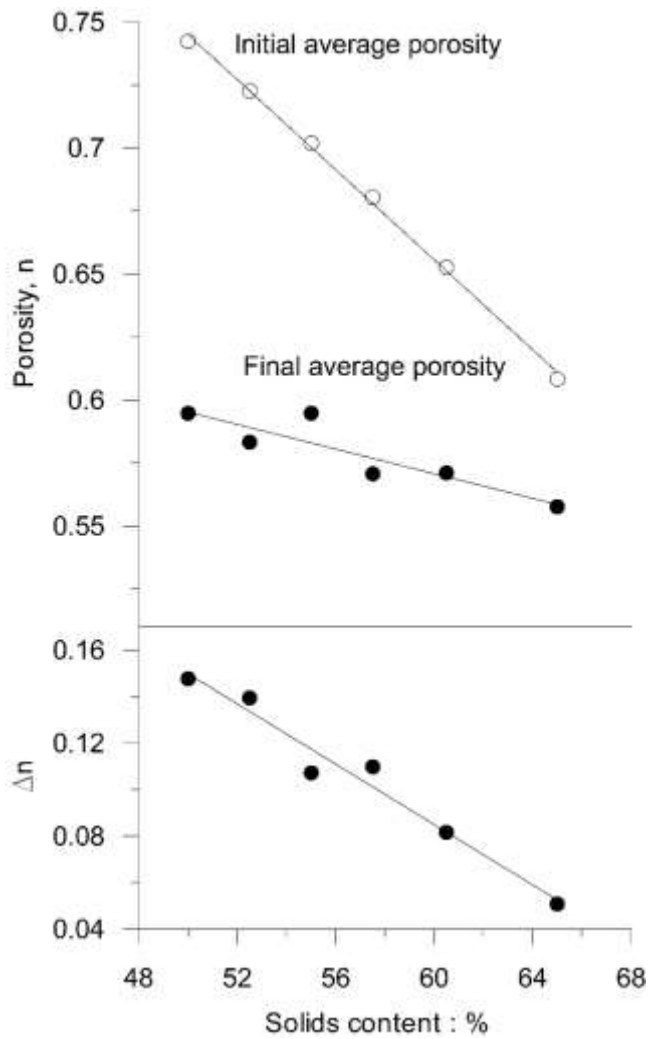
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179



180

181 Figure 5. (a) Total settlement and (b) true vertical strains as a function of solids content.



182

183 Figure 6. Initial and final average porosities for different solids content, together with changes in  
 184 porosity during sedimentation.

185

186 **3.2 Electrical measurements**

187 The electrical resistivity of soil-water slurries containing low specific surface-area particles is affected  
 188 primarily by electrolyte concentration and porosity (Santamarina et al 2001). In the work presented,  
 189 where the tailings are non-plastic, it is possible to use empirical equations, such as the one proposed  
 190 by Archie (1942), to relate the bulk resistivity of the mixture to the resistivity of the electrolyte (Klein  
 191 and Santamarina 2003).

192 For saturated rock formations the Archie relationship can be written as

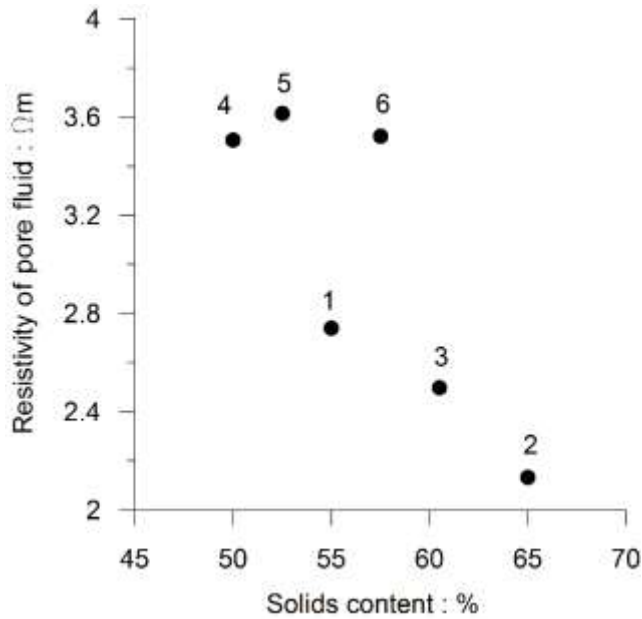
193 
$$\frac{\rho_{mix}}{\rho_{el}} = a \cdot n^{-m} \quad (2)$$

194 where  $\rho_{mix}$  is the bulk resistivity of the rock,  $\rho_{el}$  is the resistivity of the electrolyte filling the pore  
195 space,  $n$  is the porosity of the rock . The exponent  $m$  is the *cementation exponent*, and is related to the  
196 tortuosity and connectivity of the pore network within the rock and  $a$  is a correction factor, which is  
197 valid over a particular range of porosities,  $n$ . A wide range of values have been reported for  $m$  and  $a$   
198 for different rock and sediment formations, with  $a$  typically in the range 0.4 – 2.5 and  $m = 1.2 – 2.5$   
199 (e.g. Worthington 1993; Santamarina et al 2001; Khalil and Santos 2011). Values of  $a$  and  $m$  are  
200 characteristic for a given porous rock formation and are determined empirically. Archie (1942)  
201 introduced a formation resistivity factor,  $F$ , representing the resistivity magnification related to the  
202 electrolyte resulting from the presence of a non-conductive matrix (Schön 2004):

203 
$$F = \frac{\rho_{mix}}{\rho_{el}} \quad (3)$$

204 Following equation (3) above, electrical resistivity measurements made in the sedimentation column,  
205 corresponding to  $\rho_{mix}$ , were *normalised* by the resistivity of the pore-fluid  $\rho_{el}$  to derive values of the  
206 resistivity formation factor,  $F$ . The resistivity of the pore-fluid was obtained by extracting supernatant  
207 fluid at the end of a test and using the cell employed during the calibration stage. Figure 7 shows a  
208 plot of pore-fluid resistivity against solids content. The numbers above the data points indicate the  
209 order in which the tests were done.

210



211

212 Figure 7. Variation in electrical resistivity of the pore fluid with solids content. Test number indicated  
 213 above symbols.

214

215 Variations in electrical resistivity with time, recorded at each electrode level within the sedimentation  
 216 column, are presented in Figure 8. Results are given in terms of Archie's formation resistivity factor  
 217  $F$ . In addition, variations in  $F$  down the sedimentation column at the start and end of each test are  
 218 presented in Figures 9 and 10 respectively.

219 For slurries tested at solids contents of 50% and 52.5%, only measurements recorded at electrode  
 220 positions 1 and 2 (E1 and E2) are presented, as the final elevation of the slurry-water interface was at  
 221 the midpoint and just above plate electrode 3 (E3) respectively in these two tests. The equilibrium  
 222 position of the interface during the test performed at a solids content of 55% was 26mm above the top  
 223 of plate electrode 3 and the electrical field could have extended into the supernatant liquid. Hence the  
 224 final resistivity recorded at E3 in this test must be considered uncertain, especially since this is  
 225 significantly lower than values recorded at the other two electrode positions.

226 The final elevation of the slurry-water interface recorded in tests carried out at solids contents above  
 227 55% was sufficiently removed from the edge of plate electrode 3 (E3) to affect measurements. In



228 addition, in all except one test, this interface was below electrode 4, E4 (thus resulting in  $F = 1$ ); at the  
229 highest solids content of 65% the plate electrodes at position 4 were only partially covered by the end  
230 of the test. No measurements were therefore recorded at electrode position 4 in any of the tests.

231

232

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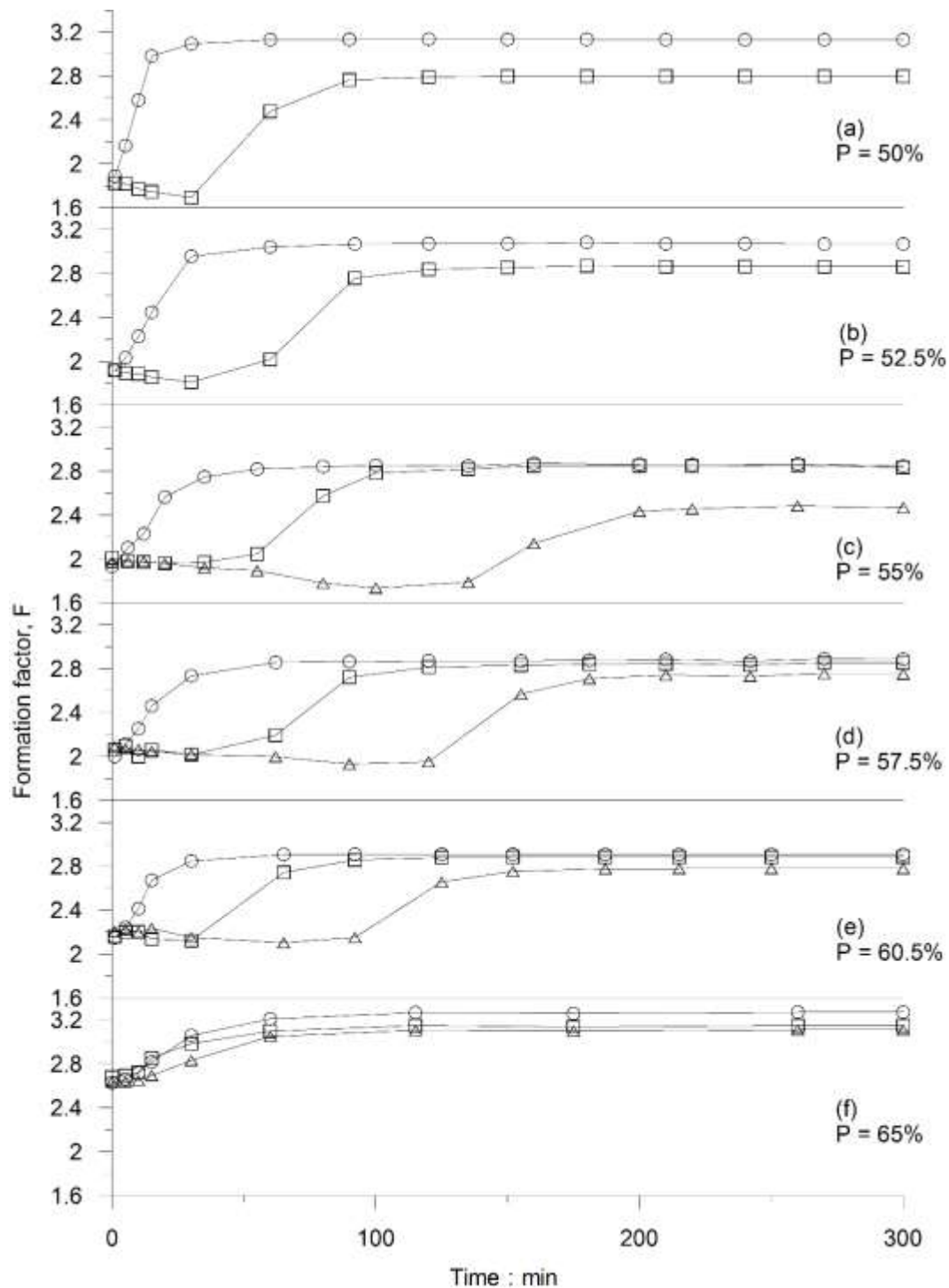
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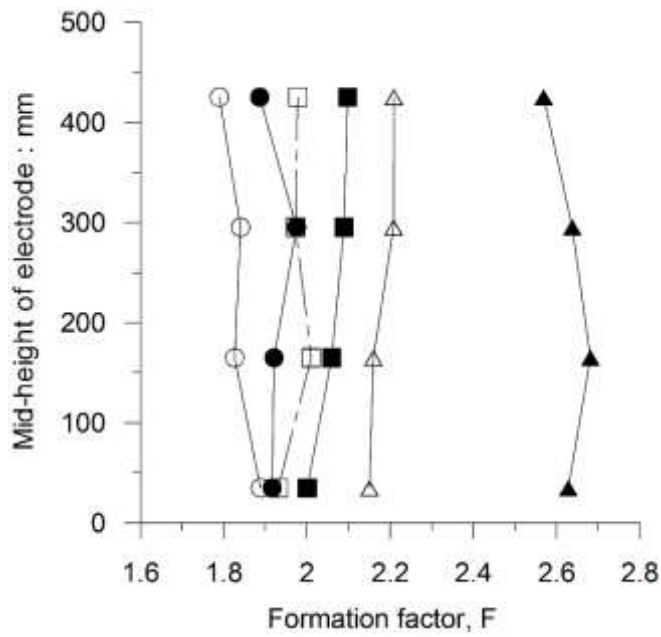
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240 Figure 8. Variation in formation resistivity factor,  $F$ , with time recorded in tests performed at solids  
 241 contents of (a) 50%, (b) 52.5%, (c) 55%, (d) 57.5%, (e) 60.5% and (f) 65%. For times in excess of  
 242 300min the response remains constant. Electrode positions (see Figure 2): E1 ( $\circ$ ), E2 ( $\square$ ), E3 ( $\Delta$ ). The  
 243 vertical scale is the same in all plots.

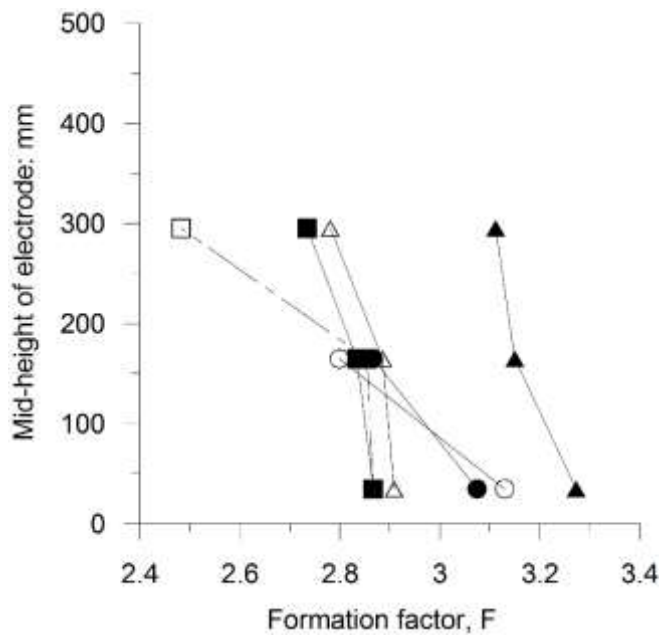
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245

246 Figure 9. Formation resistivity factor,  $F$ , plotted against depth profiles at the start of a test for different  
 247 solids contents: 50% ( $\circ$ ), 52.5% ( $\bullet$ ), 55% ( $\square$ ), 57.5% ( $\blacksquare$ ), 60.5% ( $\triangle$ ), and 65% ( $\blacktriangle$ ).

248



249

250 Figure 10. Formation resistivity factor,  $F$ , plotted against depth profiles at the end of a test (24-hours)  
 251 for different solids contents: 50% ( $\circ$ ), 52.5% ( $\bullet$ ), 55% ( $\square$ ), 57.5% ( $\blacksquare$ ), 60.5% ( $\triangle$ ), and 65% ( $\blacktriangle$ ).

252

253 **4 DISCUSSION**

254 Results presented in Figure 4 to Figure 6 reveal how, for the range of solids contents under  
255 consideration, settlements, vertical strains, initial and final porosities, as well as changes in porosity  
256 during sedimentation, vary linearly with the mass of solids in the slurry. Figure 7, on the other hand  
257 shows no correlation between resistivity of the pore fluid and solids content. The same material was  
258 used for each test, and Figure 7 only indicates an increase in pore fluid resistivity with time. Whereas  
259 values are below  $2.8\Omega\text{m}$  in earlier tests (1 to 3), these increase to approximately  $3.6\Omega\text{m}$  in latter tests  
260 (4 to 6).

261 As the formation resistivity factor vary little with depth, this indicates homogeneous conditions at the  
262 start of each test (Figure 9). However, during subsequent sedimentation the response varied according  
263 to electrode position and solids content.

264 In all tests, the formation resistivity factor at electrode position 1 (E1) increases monotonically with  
265 time to a maximum value (Figure 8), which, according to equation (2) would be the result of a  
266 decrease in porosity  $n$ . At all other electrode positions and solid contents, except for the highest  
267 (65%), the formation factor initially decreases, as the coarser particles settle, and thereafter increases  
268 as material accumulates at a particular level. This trend, however, is less evident at higher solids  
269 contents, and the effect is not observed at a solids content of 65%.

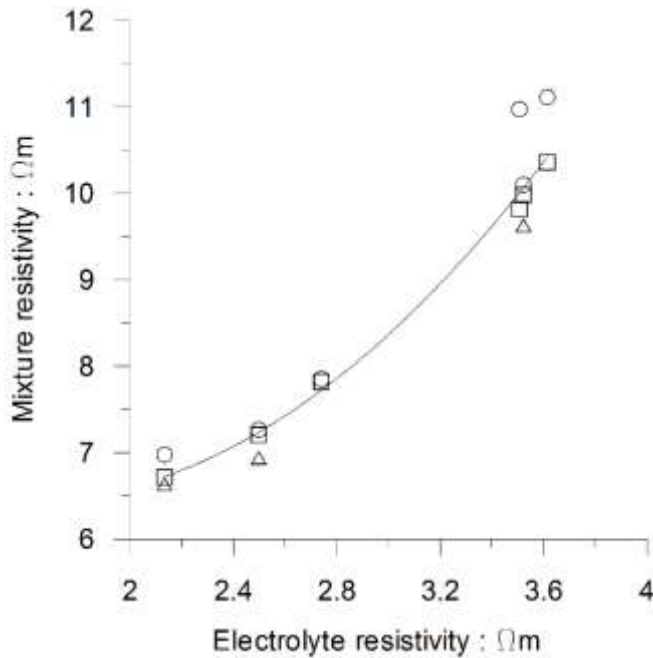
270 A comparison of the times at which settlement of the slurry-water interface ceases and formation  
271 factor stabilises reveals that, in all cases, the latter precedes the former. This is expected, as no  
272 measurements were taken above the third set of electrodes. According to equation (2), a constant  
273 value of formation resistivity factor would imply no further change in porosity.

274 The plot of the variation in formation resistivity factor,  $F$ , with depth at the end of each test (Figure  
275 10) shows that for solid contents  $\geq 57.5\%$  there is a well-defined pattern relating an increase in  $F$  with  
276 depth and solids content. For lower solids contents, although the formation factor increases with  
277 depth, the relationship with solids content does not hold. In particular, final values of formation factor  
278 measured at electrode position 1 (E1) are higher for solids contents of 50% and 52.5% than for

279 concentrations of 55% and above (with the exception of 65%). No explanation is advanced for this  
280 anomaly.

281 The variation in equilibrium bulk resistivity of the mixture with electrolyte resistivity has been plotted  
282 in Figure 11, which includes measurements recorded at each electrode level. The data has been  
283 modelled using Archie's law with  $a = 1$  and  $m = 1.95$  and is shown as a solid line. The plot reveals  
284 how pore-fluid resistivity controls bulk resistivity, as well as the effect of porosity and tortuosity on  
285 bulk resistivity.

286



287

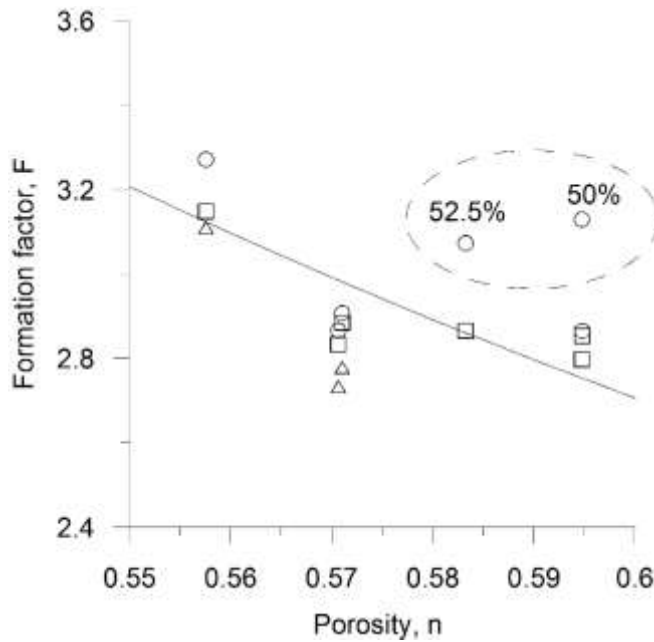
288 Figure 11. Equilibrium resistivity of the tailings mass as a function of pore fluid resistivity. Data  
289 modelled using Archie's law with  $a = 1$  and  $m = 1.95$  (solid line). Data points correspond to different  
290 electrode positions: E1 ( $\circ$ ), E2 ( $\square$ ), E3 ( $\Delta$ ).

291

292 Formation resistivity factor as a function of porosity is presented in Figure 12, together with the trend  
293 obtained using Archie's law with  $a = 1$  and  $m = 1.95$  (shown as a solid line). The experimental data  
294 can be modelled using the empirical relationship presented in equation (2) with the two highlighted

295 points excluded from the fitting equation. The latter correspond to the formation factors obtained in  
296 electrode position 1 (E1) for solid contents of 50% and 52.5%.

297



298

299 Figure 12. Formation resistivity factor as a function of porosity. Archie's law with  $a = 1$  and  $m = 1.95$   
300 represented with a solid line. Data points correspond to different electrode positions: E1 ( $\circ$ ), E2 ( $\square$ ),  
301 E3 ( $\Delta$ ). Encircled data points correspond to measurements made at E1 on samples with indicated  
302 solids content.

303

### 304 5 CONCLUDING COMMENTS

305 The main aim of this study was to assess the use of a simple experimental technique, previously  
306 employed with clay slurries, to monitor the settling and sedimentation of mine tailings. A  
307 sedimentation column, fitted with four electrode sets, was used to test slurries of solids contents over  
308 the range 50%-65%. During sedimentation, temporal changes in electrical resistivity were recorded at  
309 four electrode-set positions.

310 Test results showed a monotonic increase in resistivity with time at the base of the column; a  
311 maximum value was reached within one hour and, thereafter, resistivity remained constant. In all  
312 other electrode positions, an initial reduction in resistivity was followed by an overall increase to a  
313 constant final value. Constant resistivity is interpreted to correspond to a situation where there is no  
314 further change in the slurry porosity.

315 Bulk resistivity in particulate materials of low specific surface is controlled by the resistivity of the  
316 pore fluid and, therefore, results have been presented in terms of Archie's formation resistivity factor,  
317  $F$ , corresponding to the ratio of bulk to pore fluid resistivity. This factor represents the increase in  
318 resistivity resulting from the presence of a non-conductive matrix in an electrolyte. Slurry resistivity  
319 at equilibrium was plotted as a function of pore fluid resistivity and the data modelled using Archie's  
320 law.

321 The test performed within the sedimentation column corresponds to what is usually known as an  
322 undrained settling test. In this test, which is used to assess the rate at which supernatant fluid separates  
323 from the slurry, as well as the minimum density obtained during subaqueous deposition, only the  
324 settlement of the slurry-water interface is recorded to produce a plot similar to that shown in Figure 4.  
325 The inclusion of electrodes allows a much better understanding of spatial variation in material  
326 properties.

327 For practical reasons, tests were performed within a relatively small sedimentation column and it is  
328 acknowledged that a larger column (e.g. Been and Sills, 1981) would not only accommodate a larger  
329 number of electrodes, but it would also increase the maximum stress experienced by the slurry at the  
330 base. A combination of tests performed in larger sedimentation columns and in oedometers, such as  
331 the hydraulic oedometer described in McCarter et al (2005), could be used to derive relationships  
332 between resistivity and void ratio. This, together with in-situ measurements of electrical resistivity,  
333 could be used to monitor the sedimentation and self-weight consolidation of tailings in the field  
334 (although the consolidation stage was not investigated in the current study).

335

336 **NOTATION**

|     |              |  |
|-----|--------------|--|
| 337 | A            | electrode surface area (m <sup>2</sup> ) |
| 338 | a            | correction factor                        |
| 339 | d            | electrode separation (m)                 |
| 340 | F            | formation resistivity factor             |
| 341 | m            | cementation exponent                     |
| 342 | n            | porosity                                 |
| 343 | R            | bulk resistance (ohm)                    |
| 344 | $\rho_{el}$  | resistivity of pore fluid (ohm-m)        |
| 345 | $\rho_{mix}$ | bulk resistivity of material (ohm-m)     |

346

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350

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## Figure captions

Figure 1. Particle size distribution of the tailings sample after removal of particles retained in the 0.3mm sieve. Also shown, curves for coarse and fine gold and copper tailings from Blight (2010).

Figure 2. Sedimentation column showing location of electrodes (E1 to E4).

Figure 3. Relationship between electrolyte resistivity  $\rho$  and resistance  $R$  recorded during calibration of the sedimentation column and used to obtain the geometric constant  $A/d$  for each set of electrodes: E1 ( $\circ$ ), E2 ( $\square$ ), E3 ( $\Delta$ ) and E4 ( $\nabla$ ). Results for E2, E3 and E4 are virtually the same.

Figure 4. Vertical settlement plotted against time for different solids contents: 50% ( $\circ$ ), 52.5% ( $\bullet$ ), 55% ( $\square$ ), 57.5% ( $\blacksquare$ ), 60.5% ( $\Delta$ ), and 65% ( $\blacktriangle$ ). Settlement refers to the vertical movement of the slurry-water interface with respect to the original position of the slurry surface at the start of a test.

Figure 5. (a) Total settlement and (b) true vertical strains as a function of solids content.

Figure 6. Initial and final average porosities for different solids content, together with changes in porosity during sedimentation.

Figure 7. Variation in electrical resistivity of the pore fluid with solids content. Test number indicated above symbols.

Figure 8. Variation in formation resistivity factor,  $F$ , with time recorded in tests performed at solids contents of (a) 50%, (b) 52.5%, (c) 55%, (d) 57.5%, (e) 60.5% and (f) 65%. For times in excess of 300min the response remains constant. Electrode positions (see Figure 2): E1 ( $\circ$ ), E2 ( $\square$ ), E3 ( $\Delta$ ). The vertical scale is the same in all plots.

Figure 9. Formation resistivity factor,  $F$ , plotted against depth profiles at the start of a test for different solids contents: 50% ( $\circ$ ), 52.5% ( $\bullet$ ), 55% ( $\square$ ), 57.5% ( $\blacksquare$ ), 60.5% ( $\Delta$ ), and 65% ( $\blacktriangle$ ).

Figure 10. Formation resistivity factor,  $F$ , plotted against depth profiles at the end of a test (24-hours) for different solids contents: 50% ( $\circ$ ), 52.5% ( $\bullet$ ), 55% ( $\square$ ), 57.5% ( $\blacksquare$ ), 60.5% ( $\Delta$ ), and 65% ( $\blacktriangle$ ).

Figure 11. Equilibrium resistivity of the tailings mass as a function of pore fluid resistivity. Data modelled using Archie's law with  $a = 1$  and  $m = 1.95$  (solid line). Data points correspond to different electrode positions: E1 ( $\circ$ ), E2 ( $\square$ ), E3 ( $\Delta$ ).

Figure 12. Formation resistivity factor as a function of porosity. Archie's law with  $a = 1$  and  $m = 1.95$  represented with a solid line. Data points correspond to different electrode positions: E1 ( $\circ$ ), E2 ( $\square$ ), E3 ( $\Delta$ ). Encircled data points correspond to measurements made at E1 on samples with indicated solids content.